

Catalysis in hydrogen production and storage



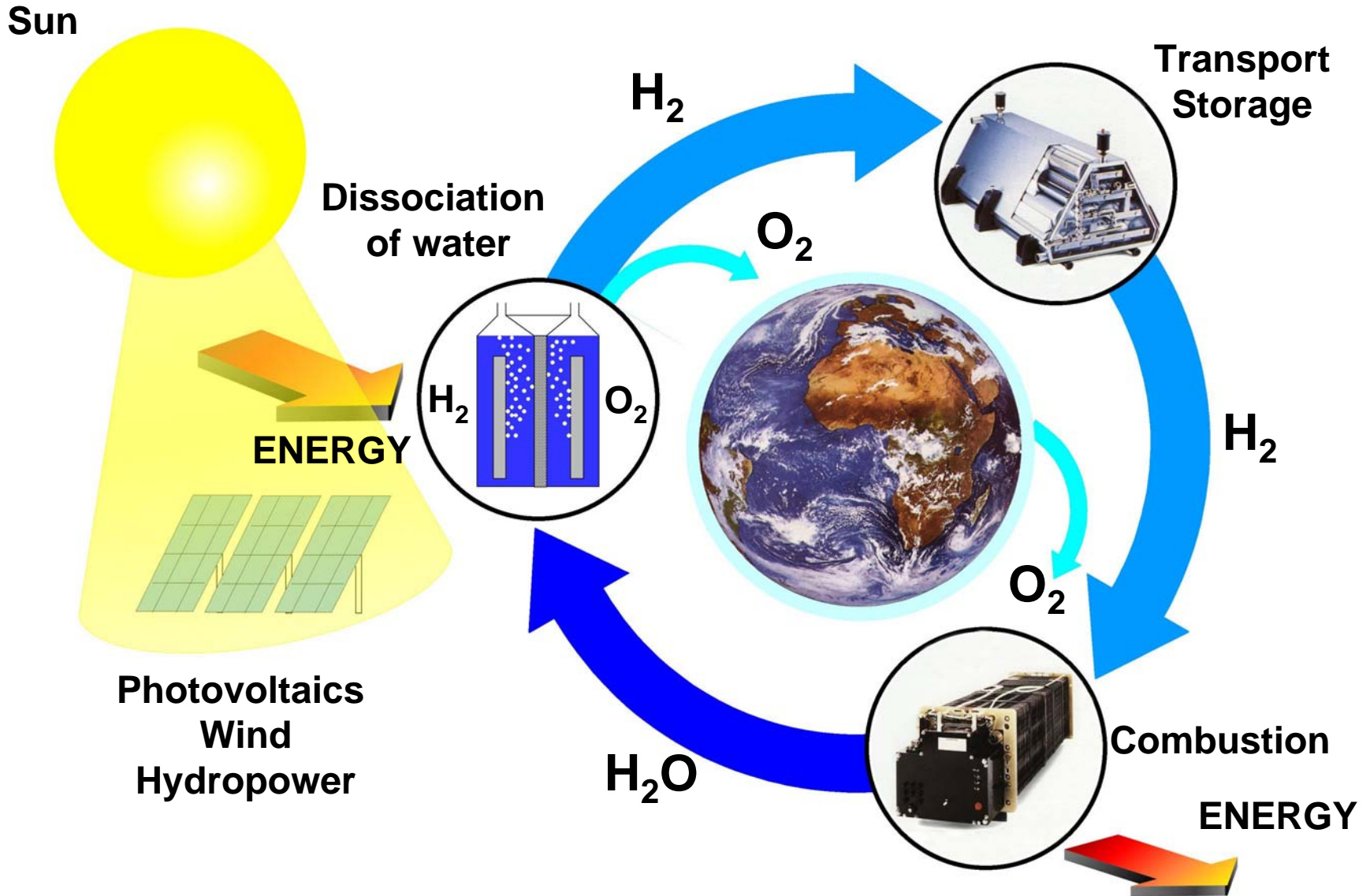
J. K. Nørskov

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Technical University of Denmark

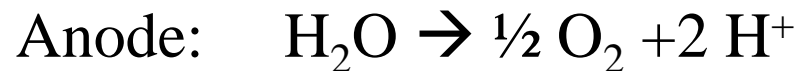
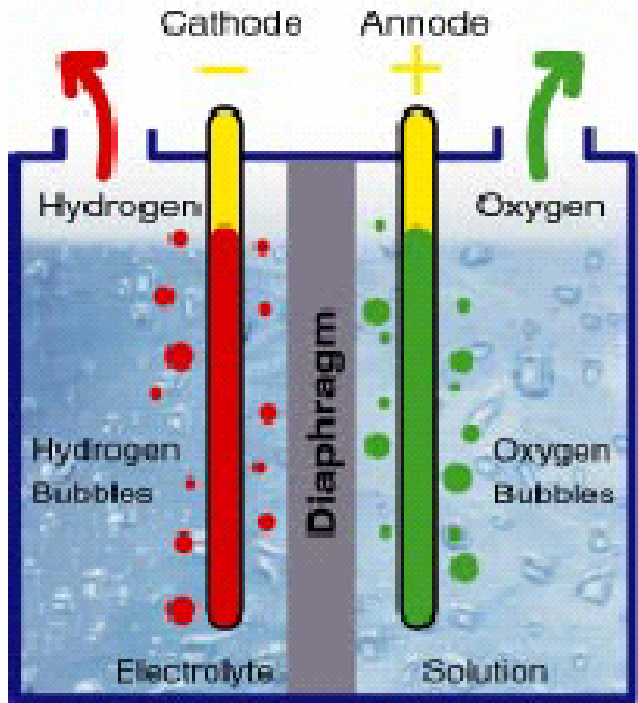
norskov@fysik.dtu.dk

- Catalysis in hydrogen production
 - Theory: J. Rossmeisl, J. Greeley, T. Bligaard, B. Hinnemann, P.G. Moses
 - Experiment: T. Jaramillo, J. Bonde, K. Jørgensen, J. Nielsen, S.Horch, I. Chorkendorff
- Catalysis in hydrogen storage
 - Theory: J. Hummelshøj, T. Vegge, K. Honkala
 - Experiment: C. Christensen, T. Johannesen, R. Z. Sørensen, U. Quaade

Sustainable hydrogen production

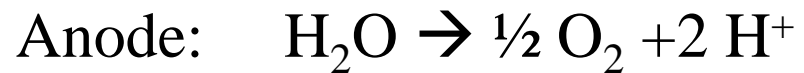
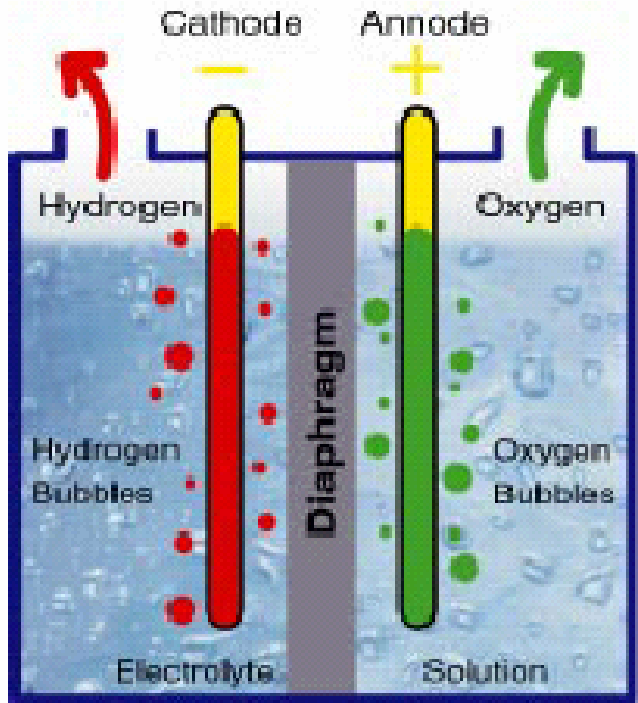


Electrolysis



$$\Delta G^0 = 2.46 \text{ eV} \quad (1.23 \text{ eV/electron})$$

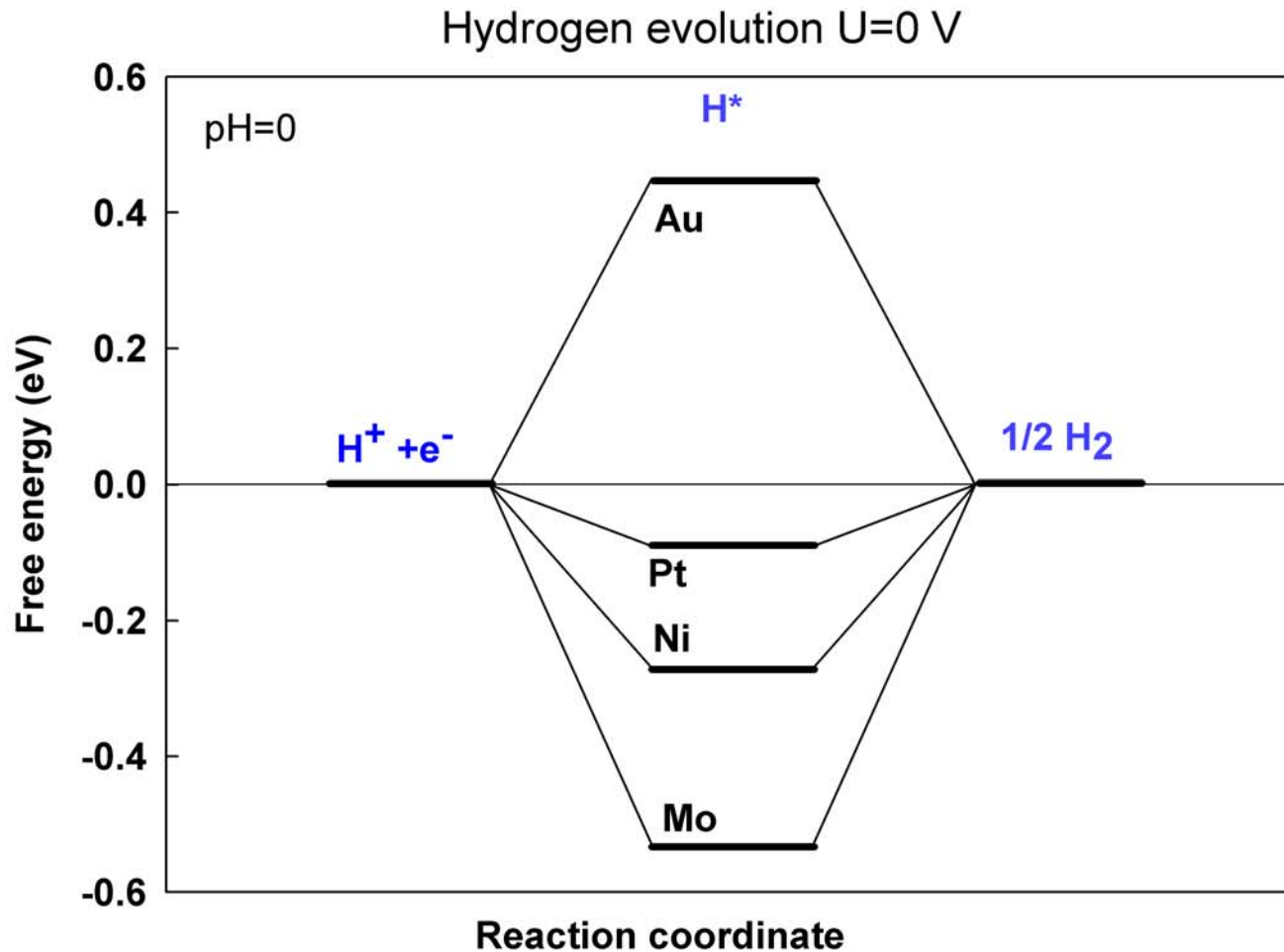
Electrolysis



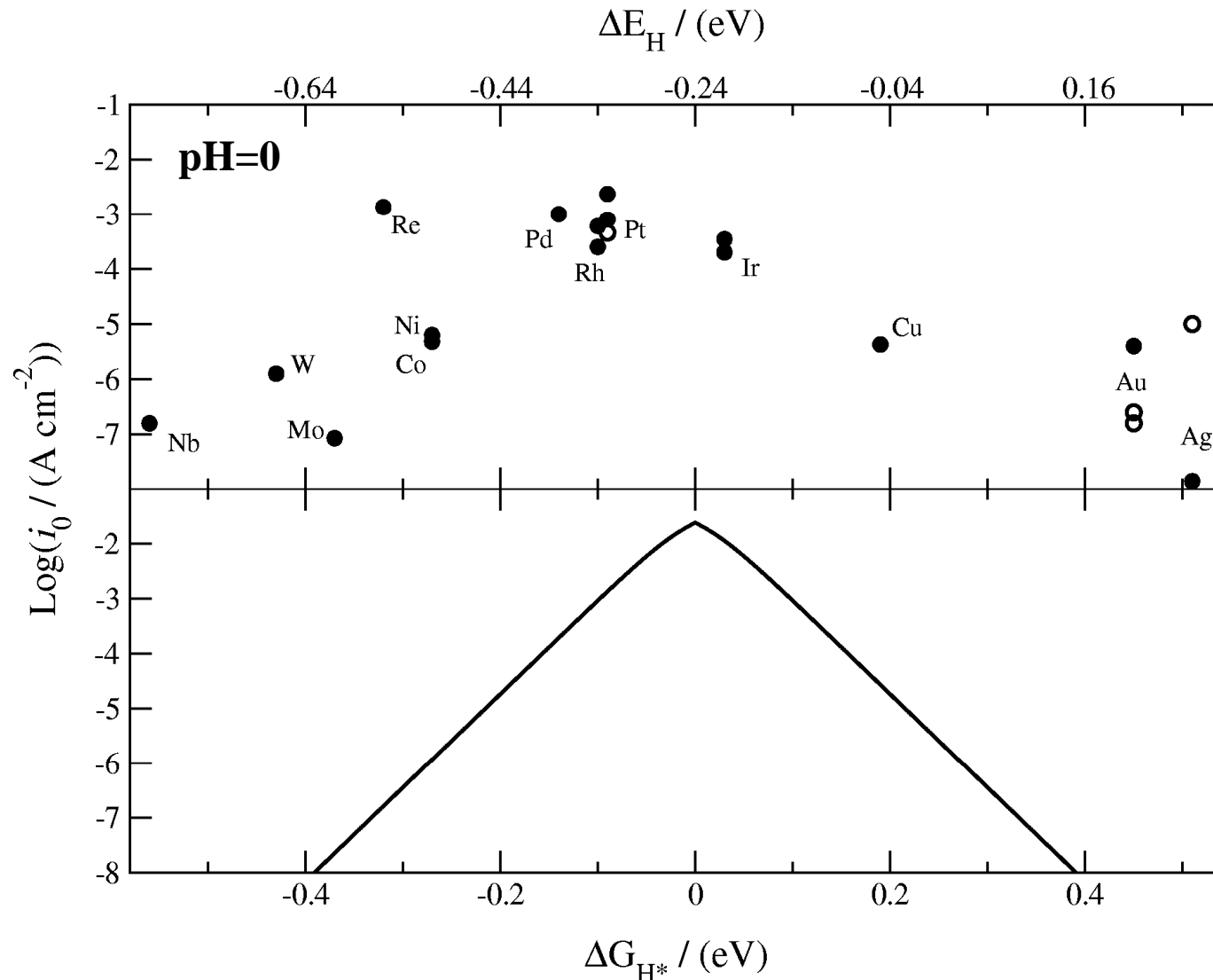
$\Delta G^0 = 2.46 \text{ eV}$ (1.23 eV/electron)

The hydrogen evolution process

DFT calculations give free energy of intermediates:



Using DFT energies in volcano



Volcanoes in electrochemistry

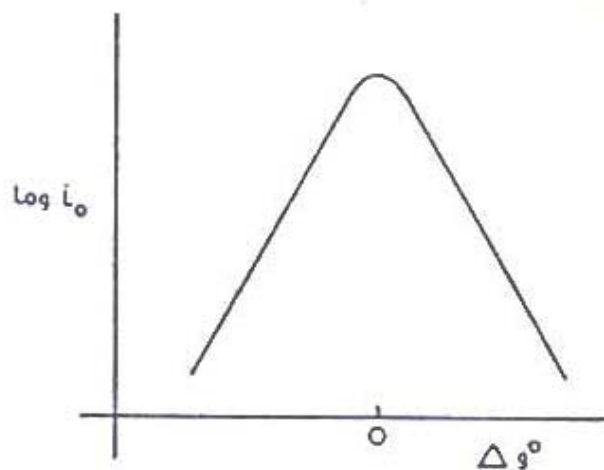
THE RATE OF ELECTROLYTIC HYDROGEN EVOLUTION AND THE HEAT OF ADSORPTION OF HYDROGEN

BY ROGER PARSONS

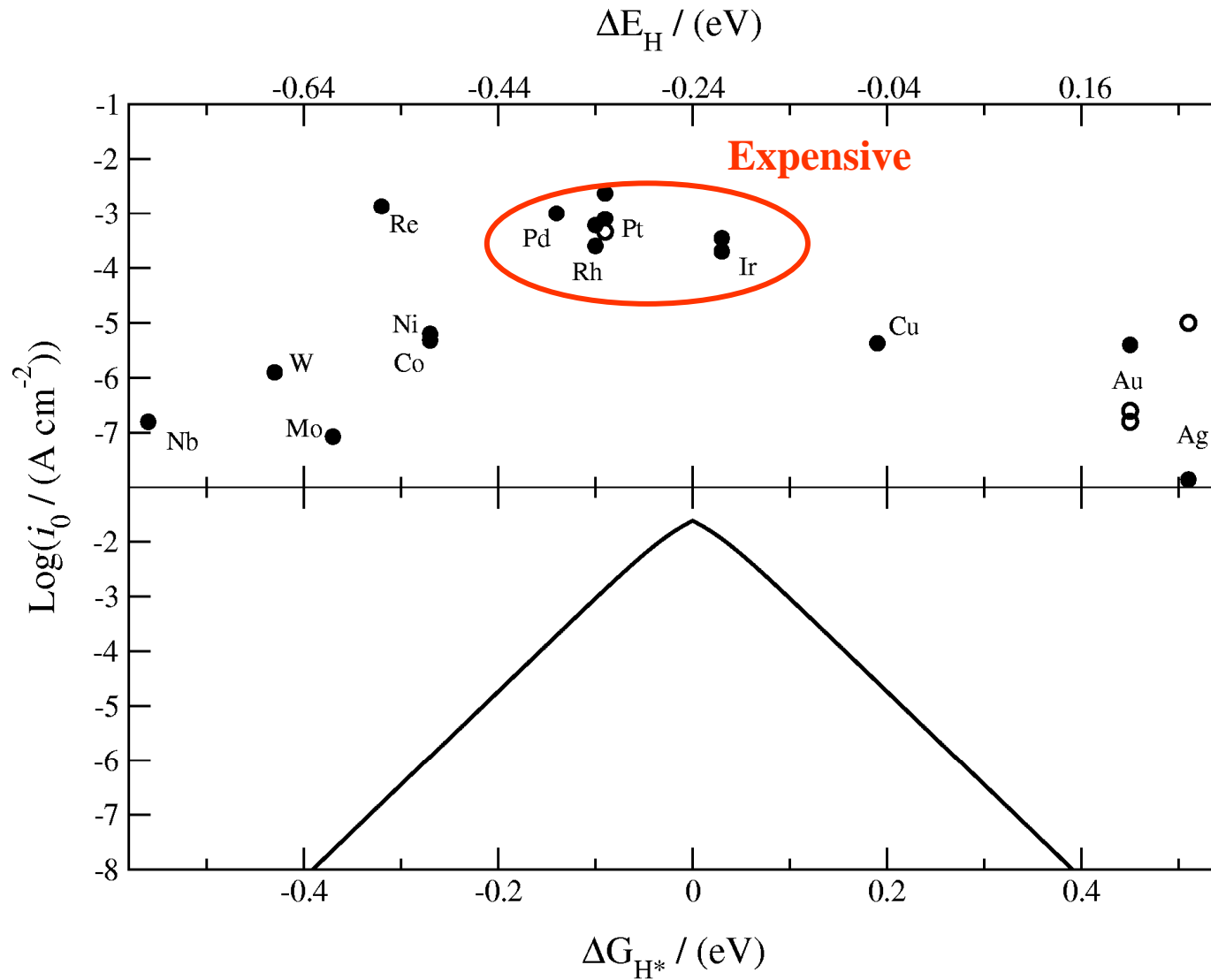
Dept. of Physical and Inorganic Chemistry, The University, Bristol 8

Received 10th December, 1957

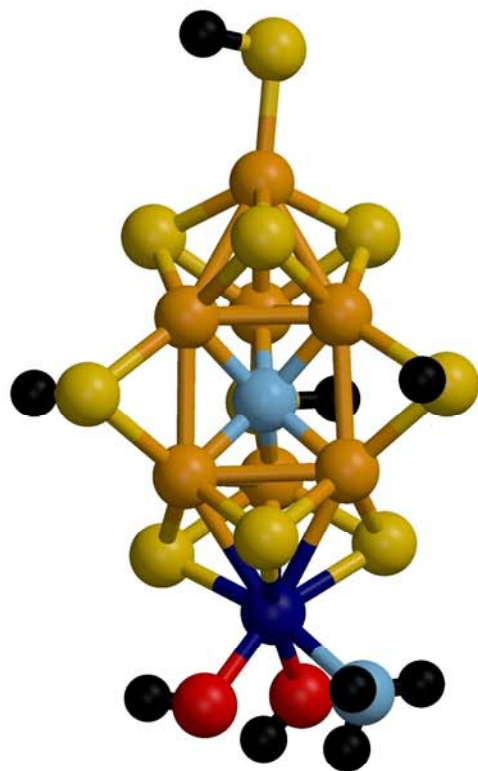
FIG. 1.—Form of the relation between exchange current at a hydrogen electrode and the standard free energy of adsorption of hydrogen on the electrode surface, assuming that the adsorbed atoms obey a Langmuir adsorption isotherm.



HER volcano



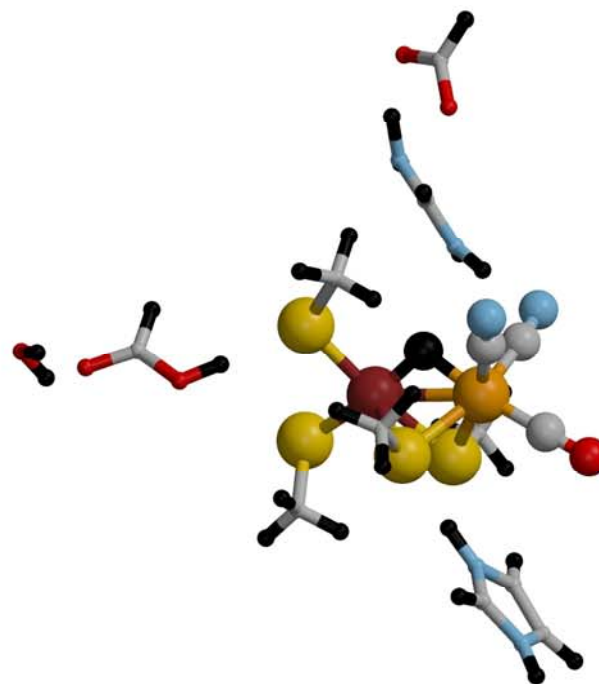
Active sites of hydrogen producing enzymes



nitrogenase
active site

Einsle, Teczan, Andrade, Schmid, Yoshida, Howard, Rees, *Science* **2002**, 297, 1696.

Hinnemann, Nørskov, *JACS* **126**, 3920 (2004)



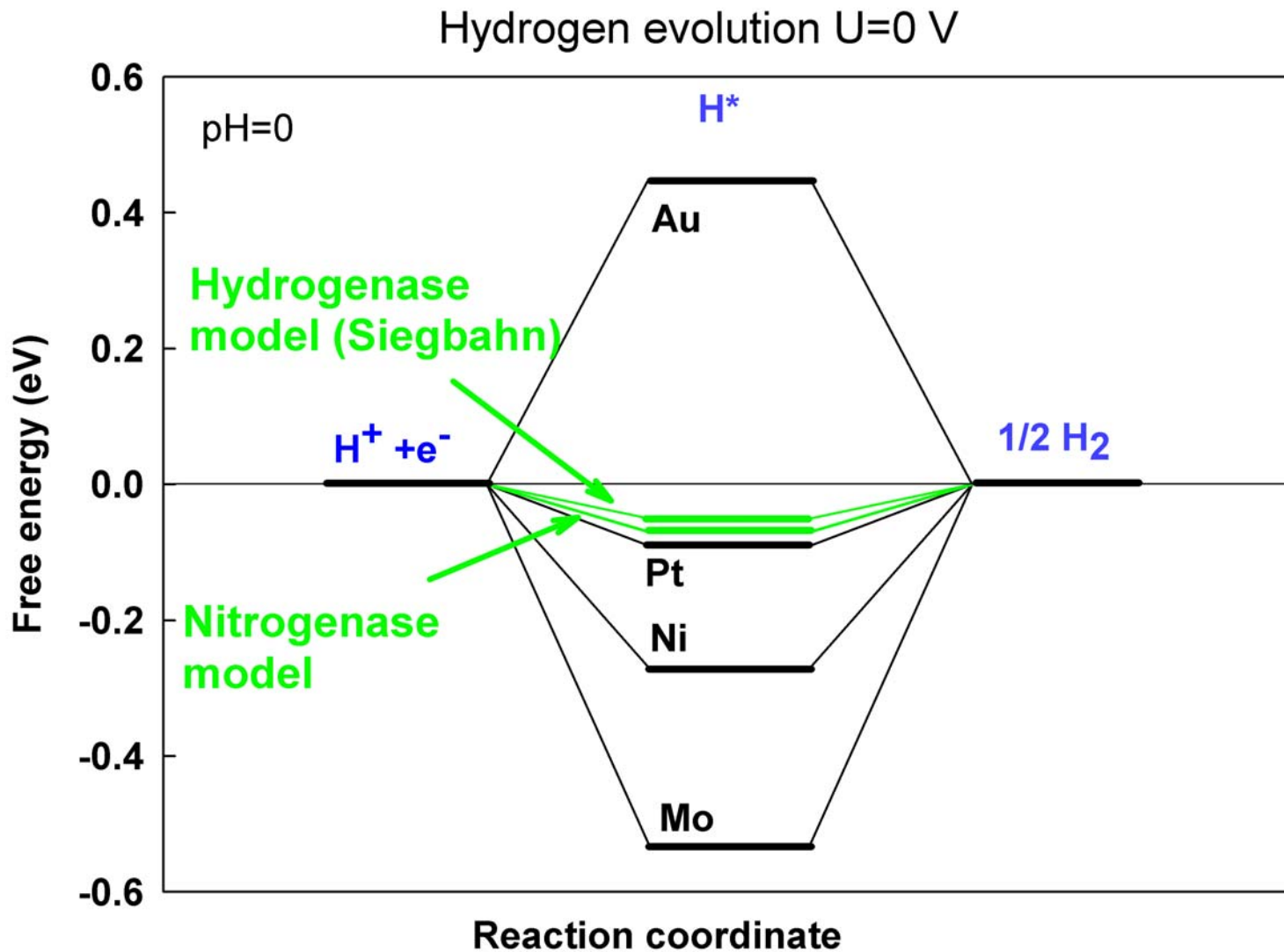
hydrogenase
active site

Vollbeda, Fontecilla-Camps, *Dalton Trans.* 4030-3048 (2003).

Siegbahn, Blomberg, Wirstam, Crabtree *Biol. Inorg. Chem.* **6**, 460 (2001)

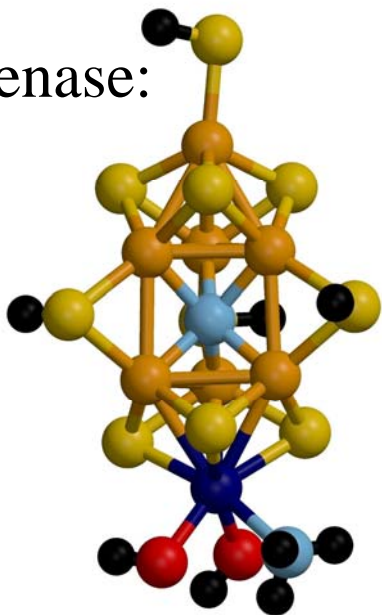


Biological hydrogen evolution

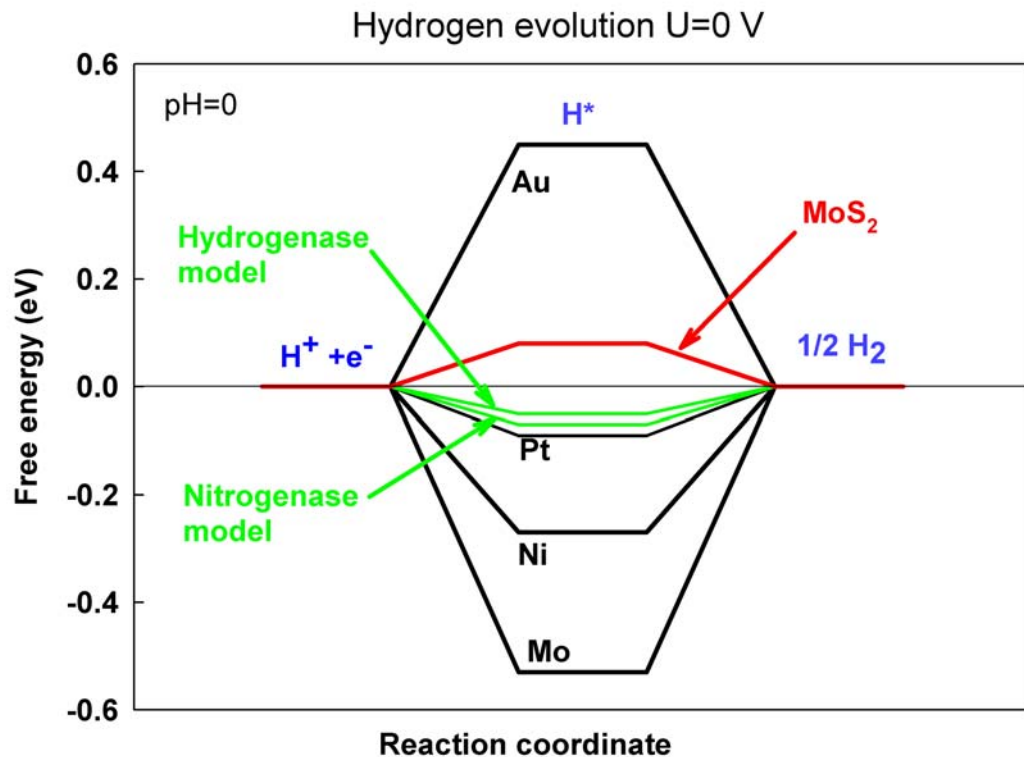
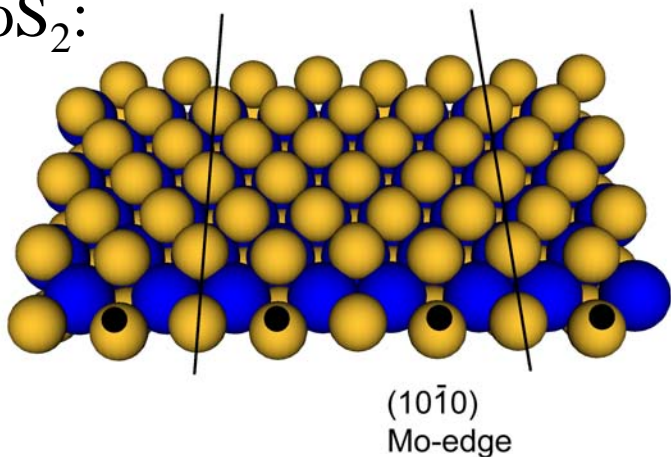


MoS₂ as HER catalyst

Nitrogenase:

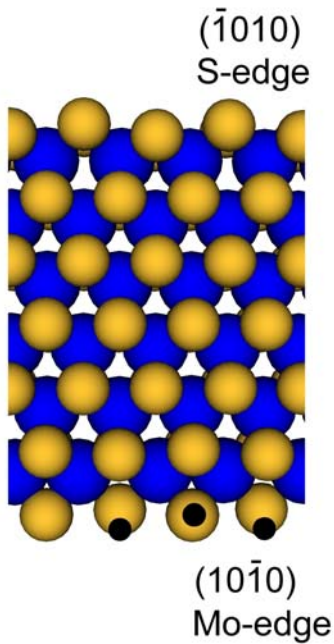


MoS₂:

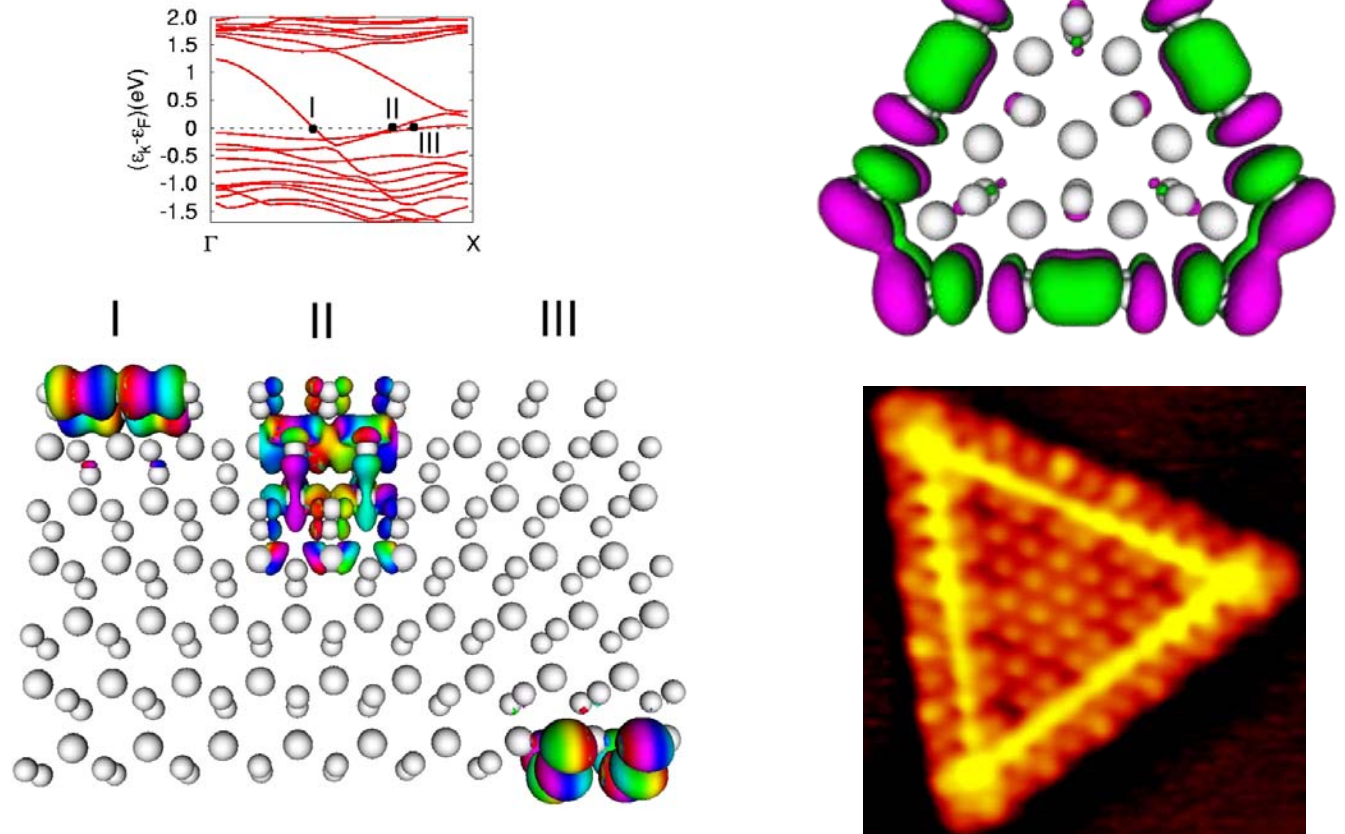


MoS₂ nanoparticles are metallic

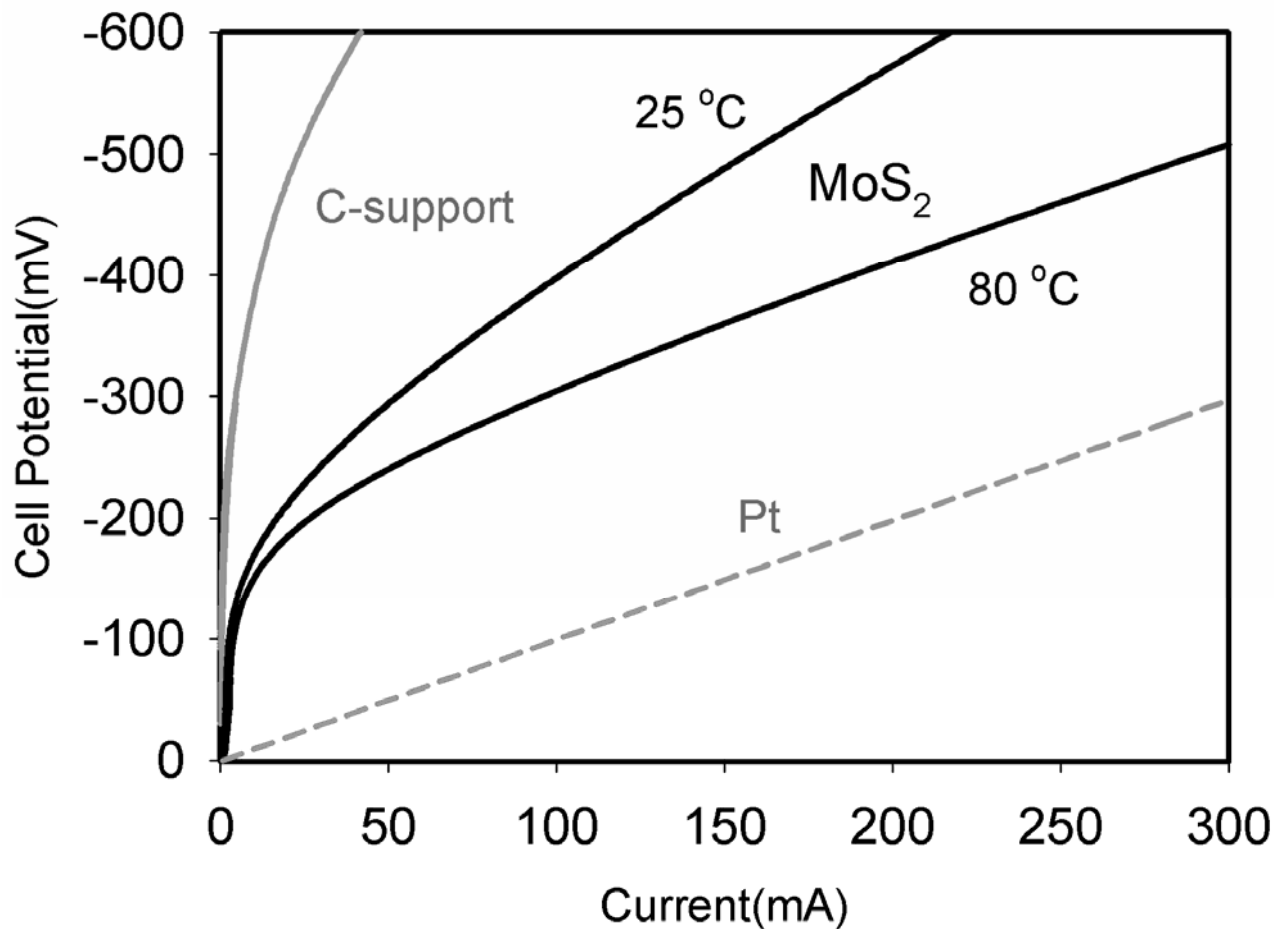
1-layer slab:



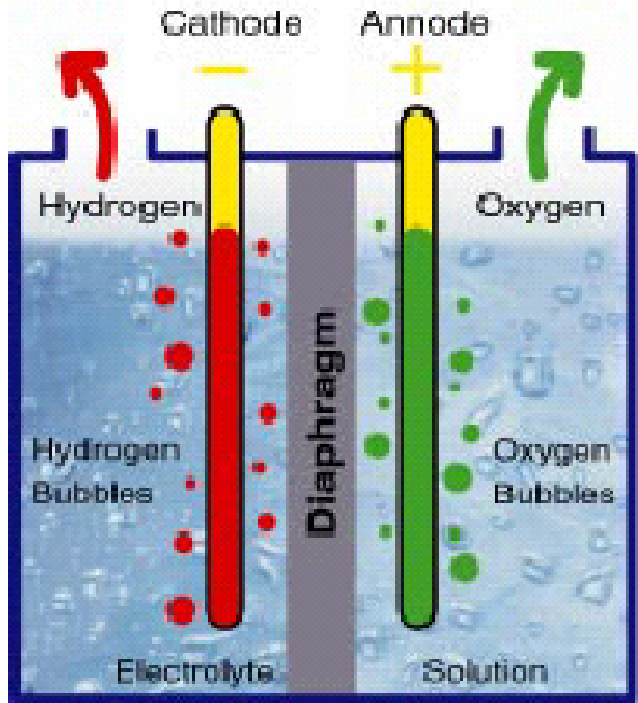
Nanoparticles:



MoS₂ as HER catalyst

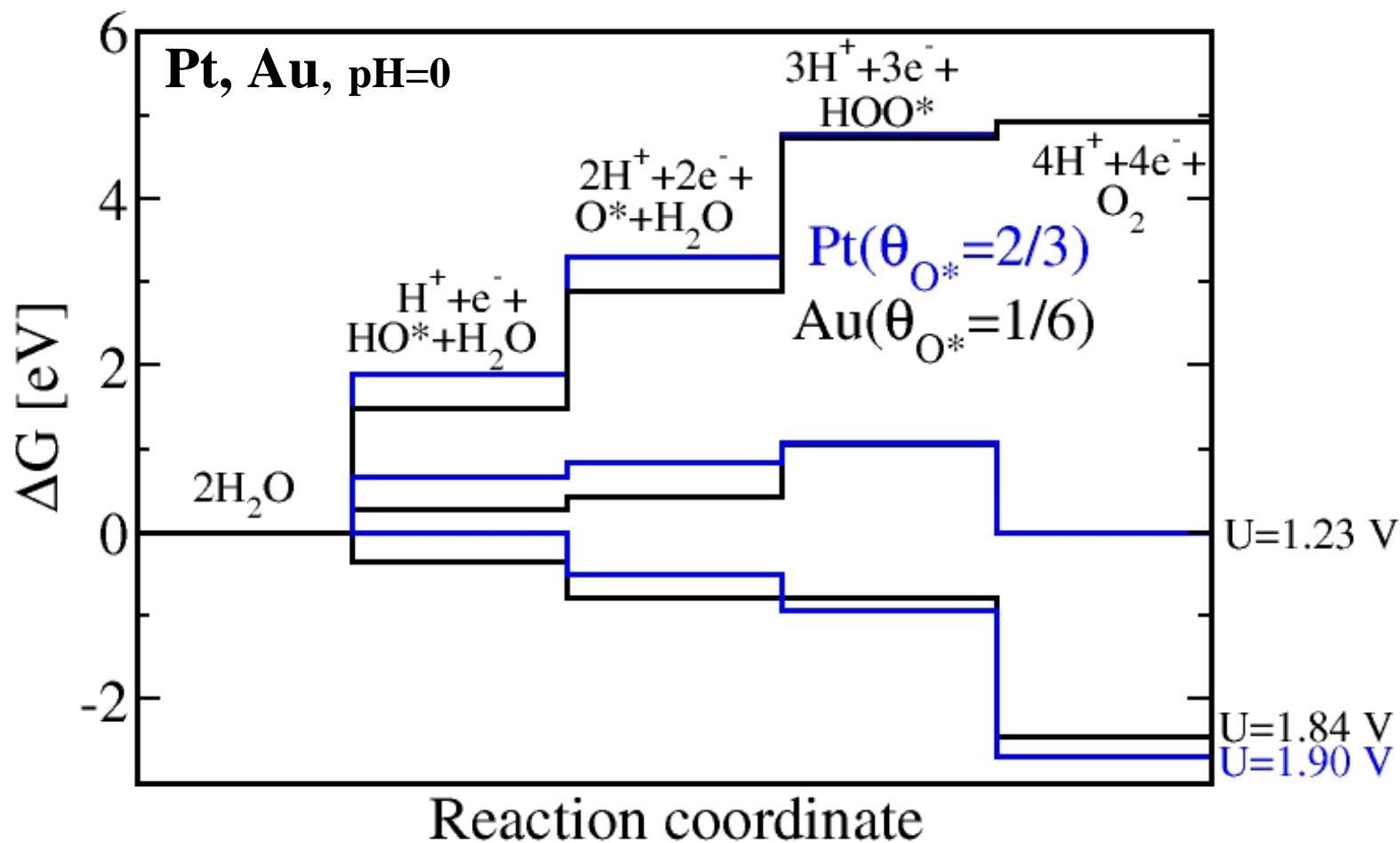


Electrolysis

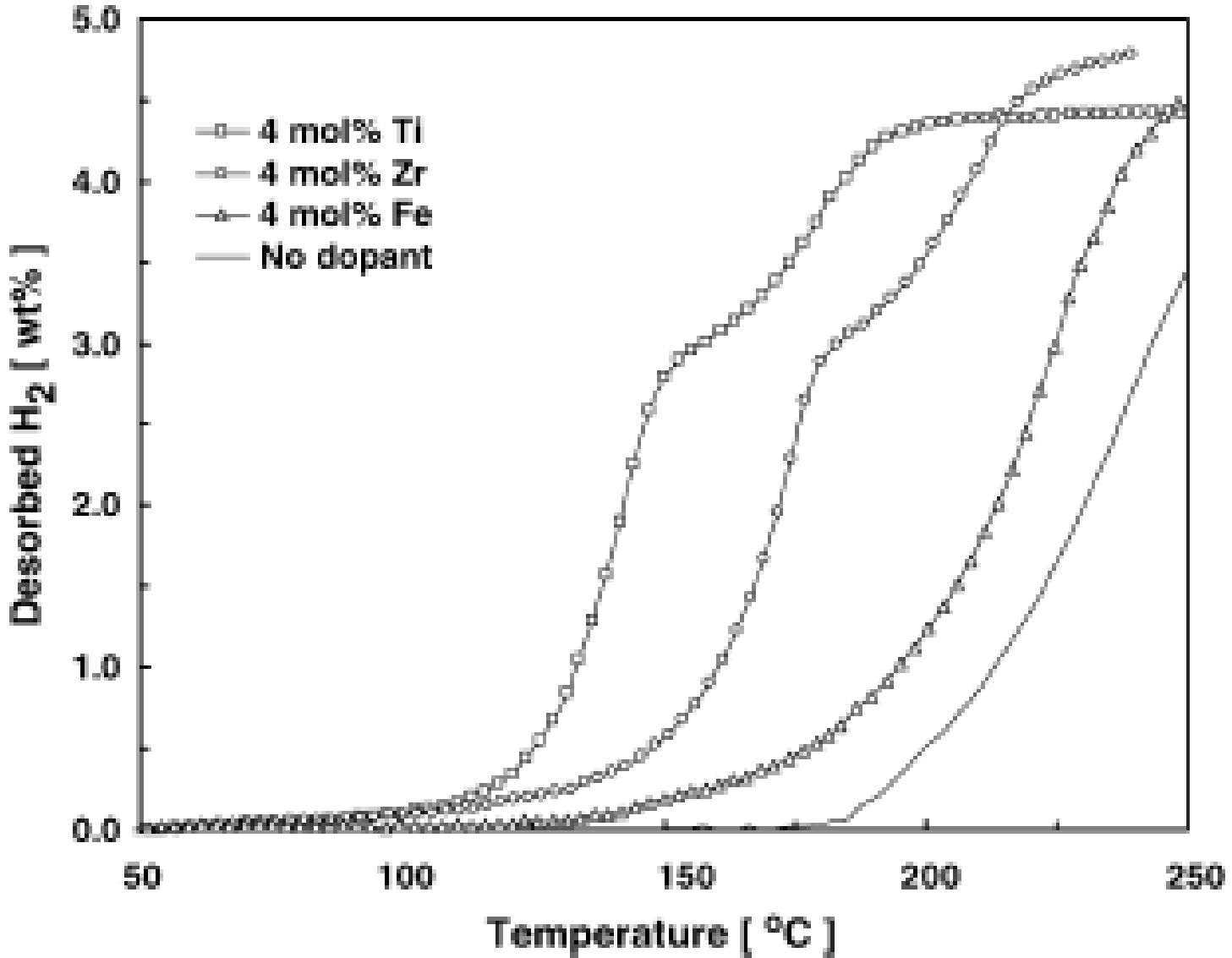


$$\Delta G^0 = 2.46 \text{ eV} \quad (1.23 \text{ eV/electron})$$

Water splitting at different potentials



Catalyzed decomposition of NaAlH_4



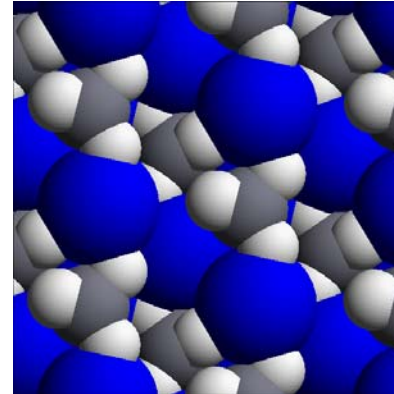
Catalyzed formation/decomposition of NaAlH_4

T. Vegge:

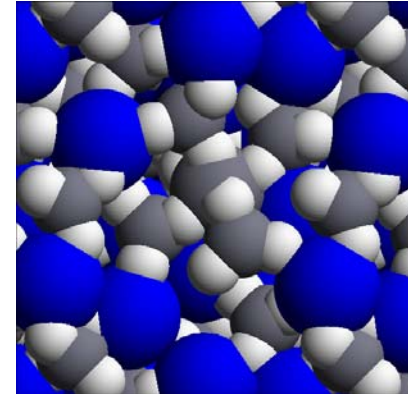
TiCl_3 as catalyst:

- lowers the H_2 desorption barrier
- Na/H-vacancy formation energy
- driving force: NaCl formation
- Ti- has long range effects

$\text{NaAlH}_4(001)$

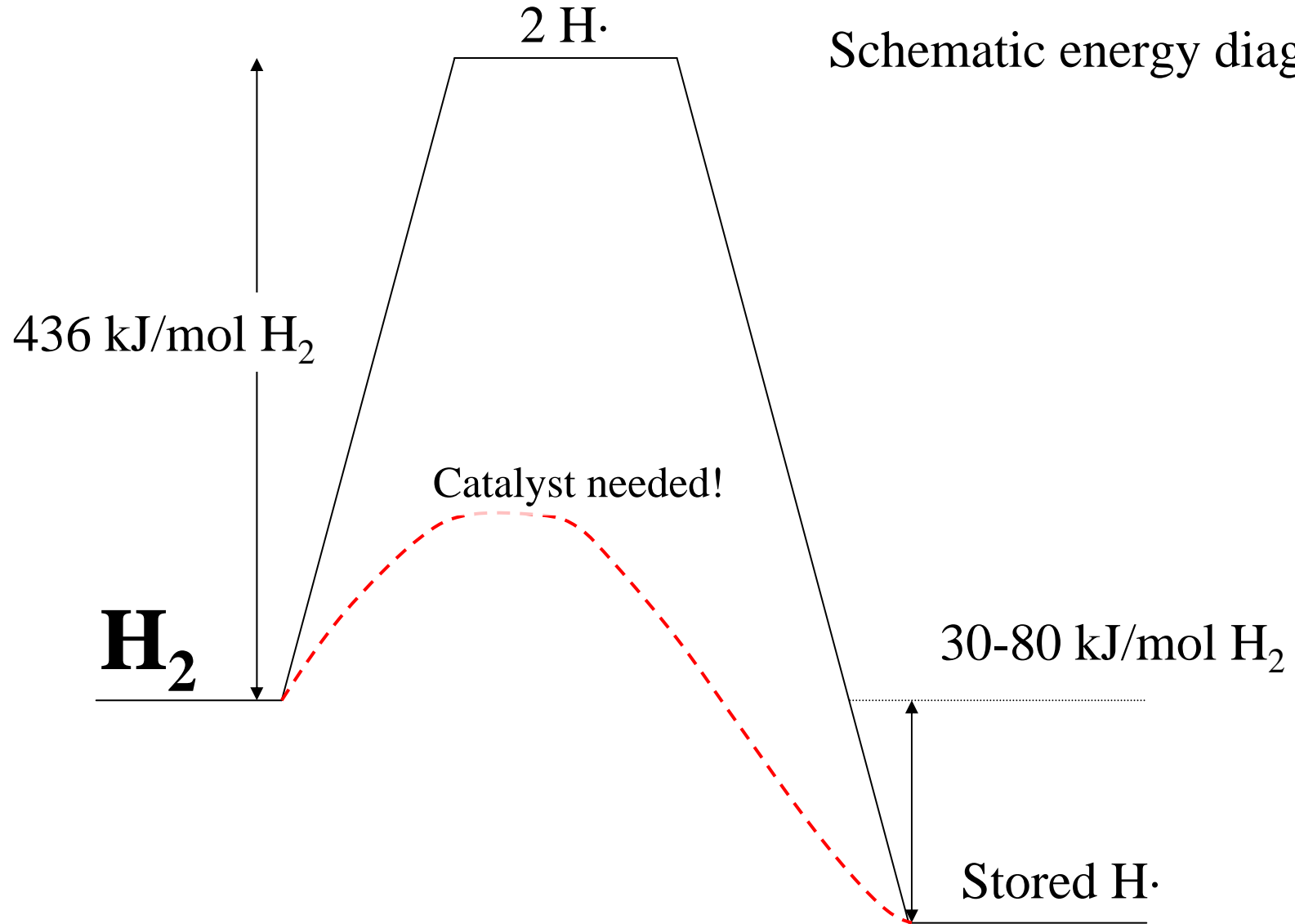


$\text{Ti@NaAlH}_4(001)+2\text{Na}^\vee$



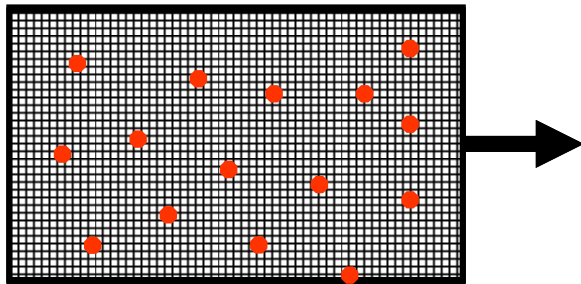
Activating H_2

Schematic energy diagram

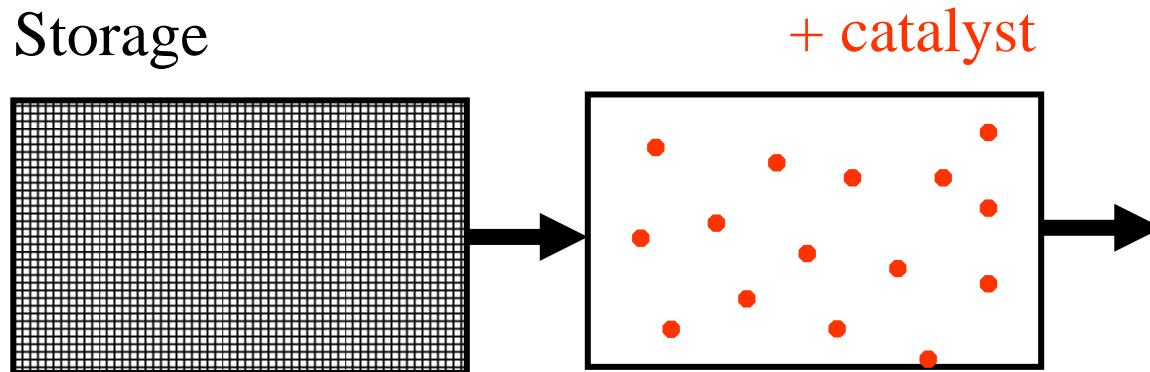


Separating storage and catalyst

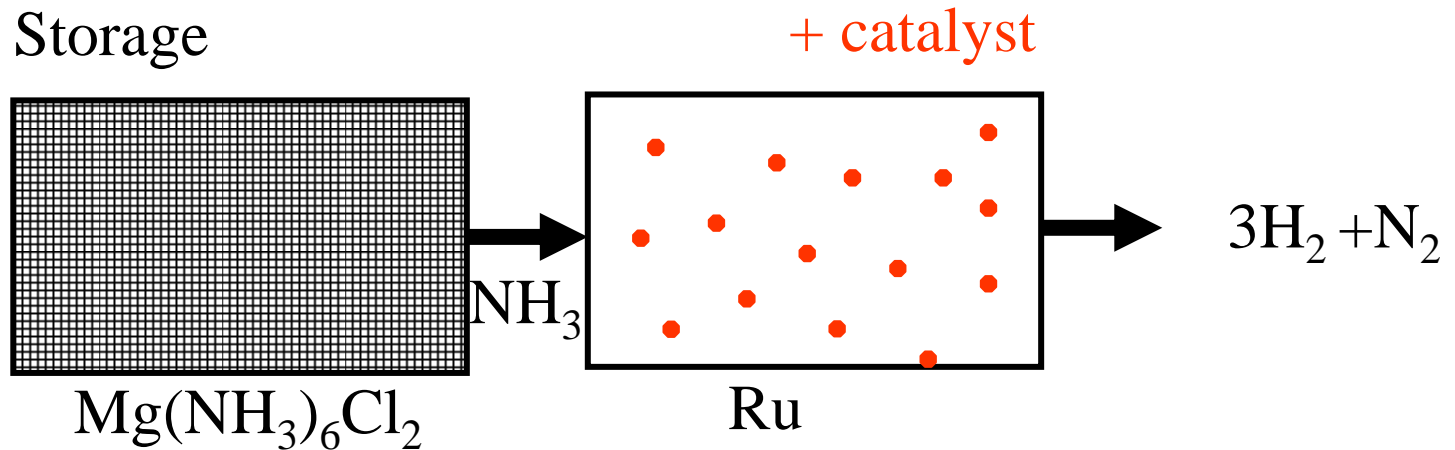
Storage + catalyst



Separating storage and catalyst



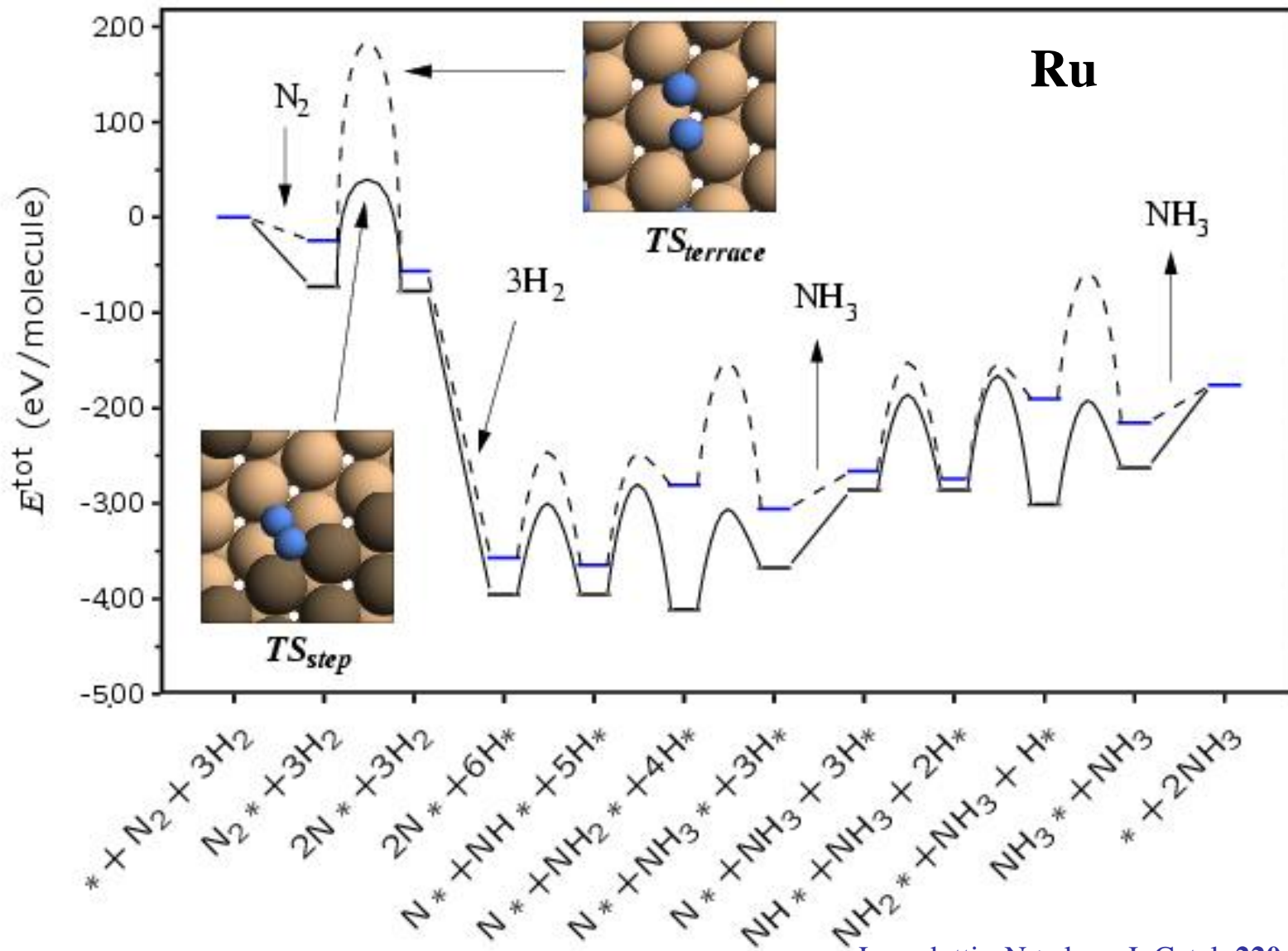
Separating storage and catalyst



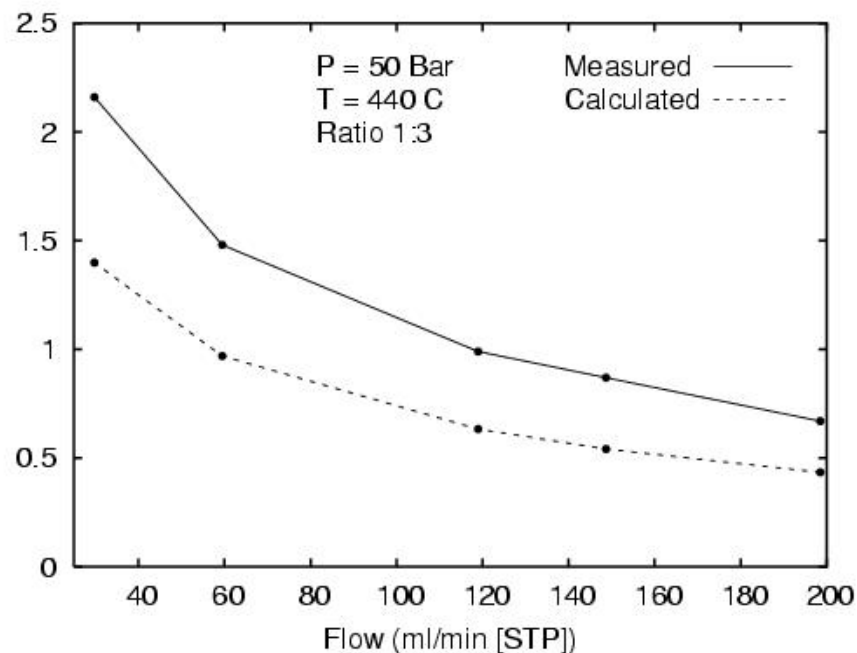
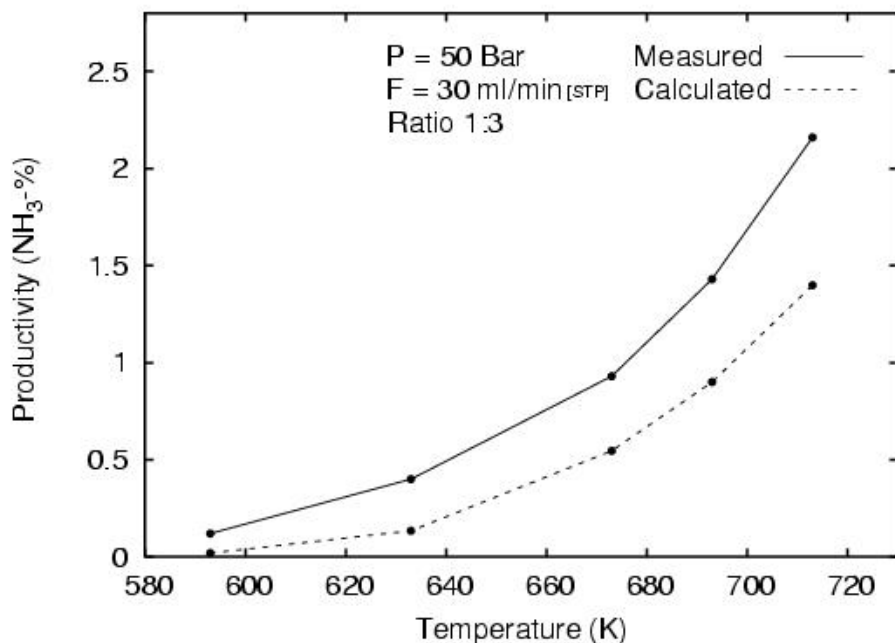
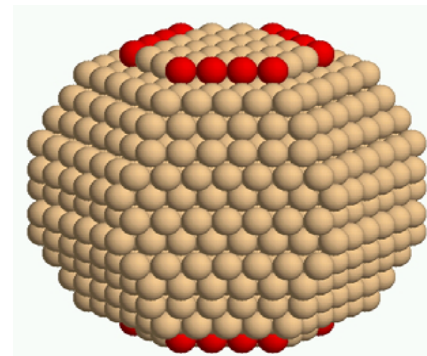
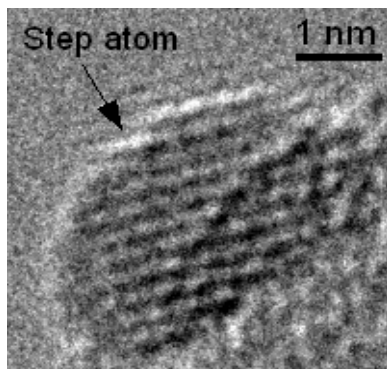
One possibility: Use metal ammine complexes

Christensen, Sørensen, Johannessen,
Quaade, Honkala, Elmøe, Køhler, Nørskov,
J. Mater. Chem **15**, 1406 (2005)

Catalyzed synthesis/decomposition of ammonia

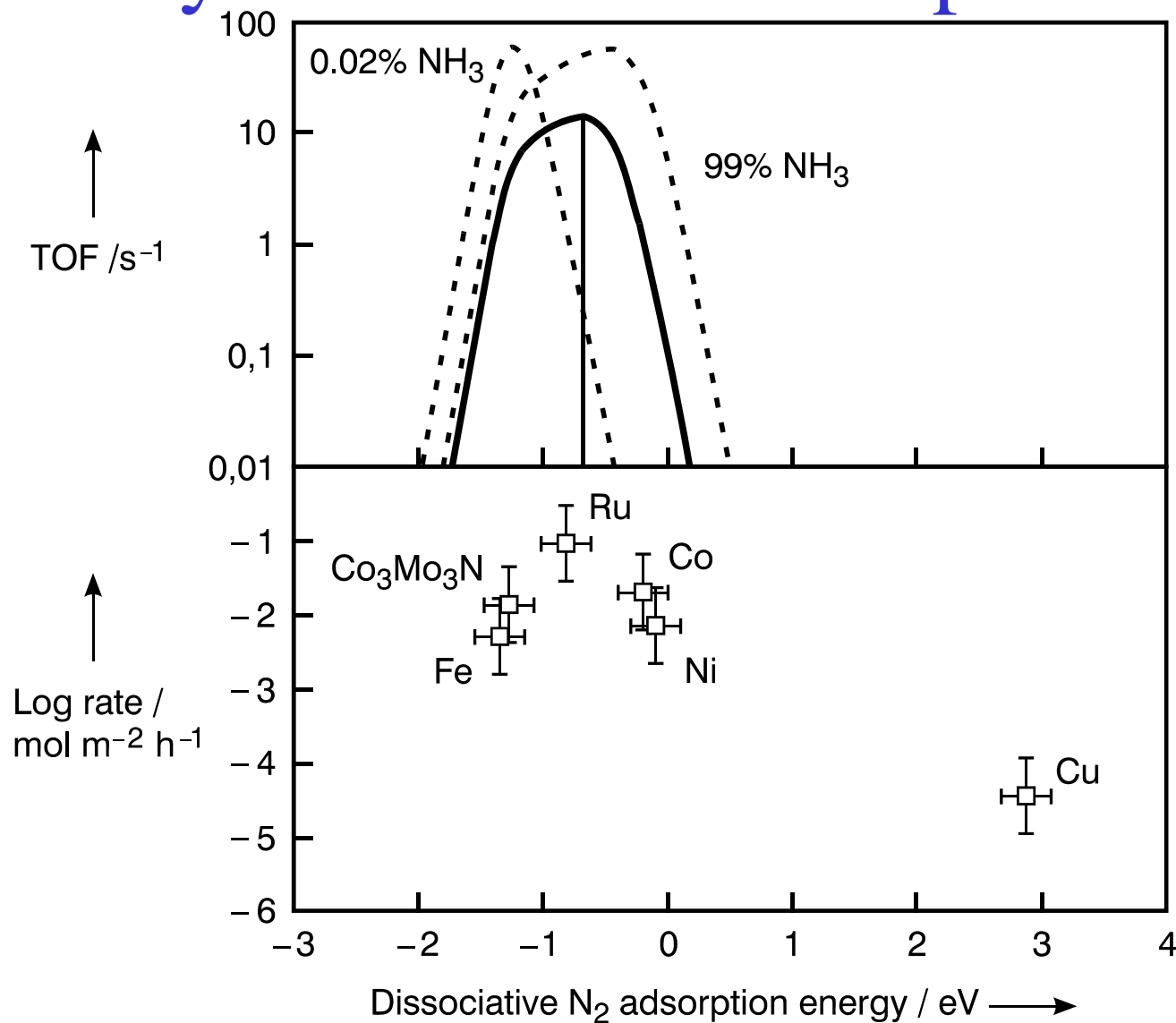


Ab initio kinetics – Ru catalysts



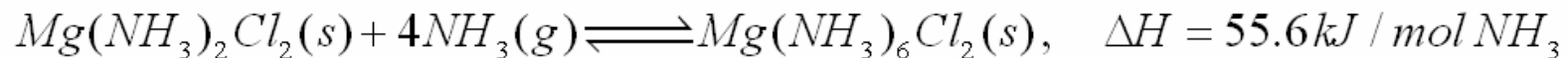
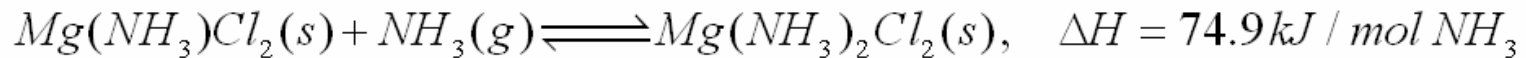
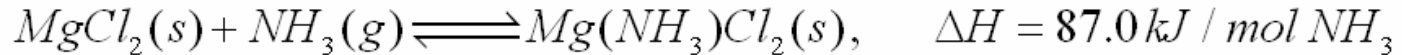
Honkala, Remediakis, Logadottir, Nørskov, Hellmann, Dahl, Carlsson, Christensen, *Science* **307**,555 (2005)

Optimal catalyst for ammonia synthesis and decomposition



Metal ammine chemistry

– the $MgCl_2-NH_3$ system



Average desorption enthalpy: $42.7 \frac{\text{kJ}}{\text{mol } H_2}$

A. Werner, “On the constitution and configuration of higher-order compounds”, 1913.

E. Lepinasse and B. Spinner, Rev. Int. Froid, 1994, 17, 309.

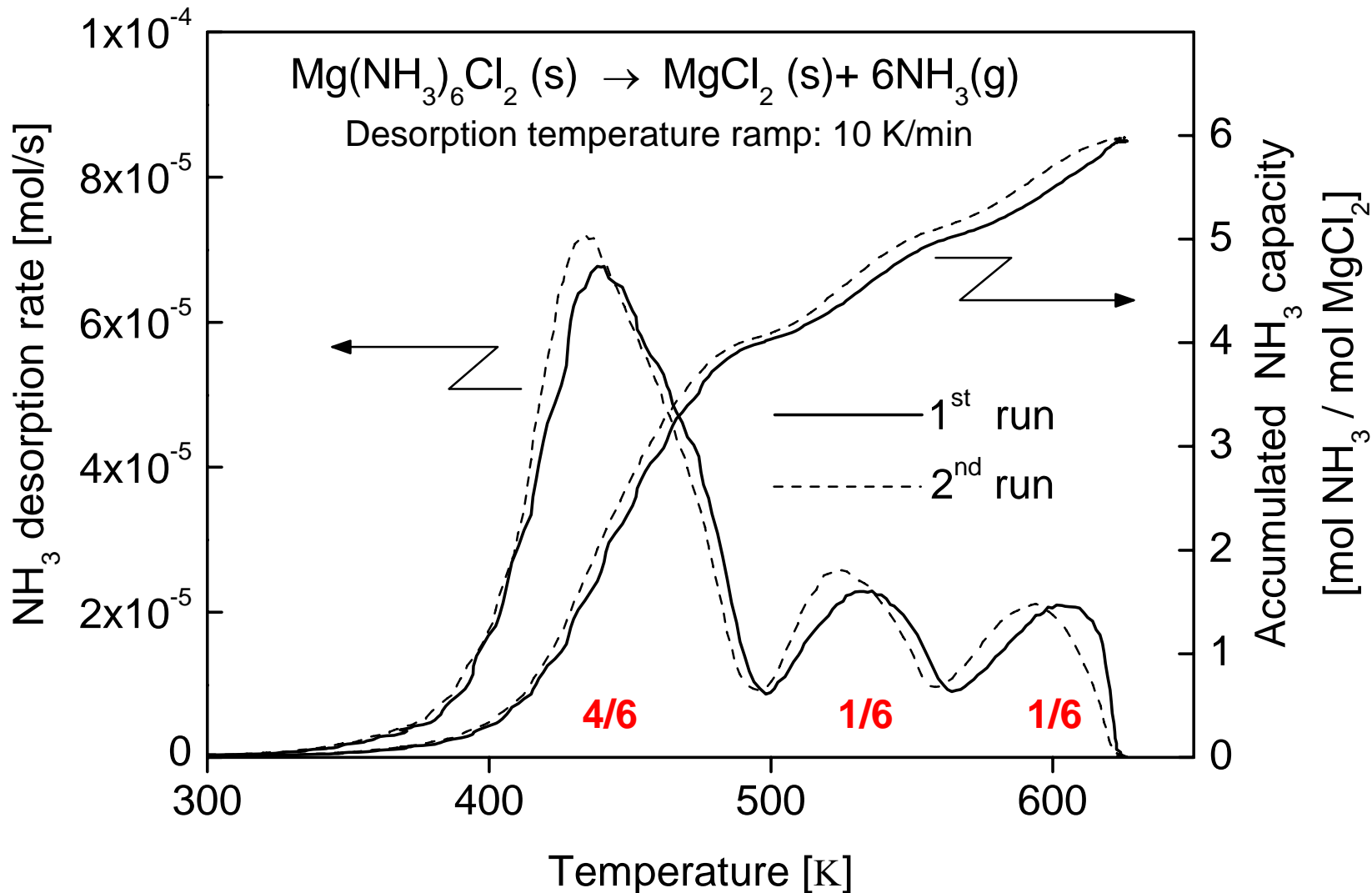
Bulk properties

$MgCl_2$:	2325 kg/m ³ ;	40,9 cm ³ /mol
$Mg(NH_3)_6Cl_2$:	1252 kg/m ³ ;	157,4 cm ³ /mol

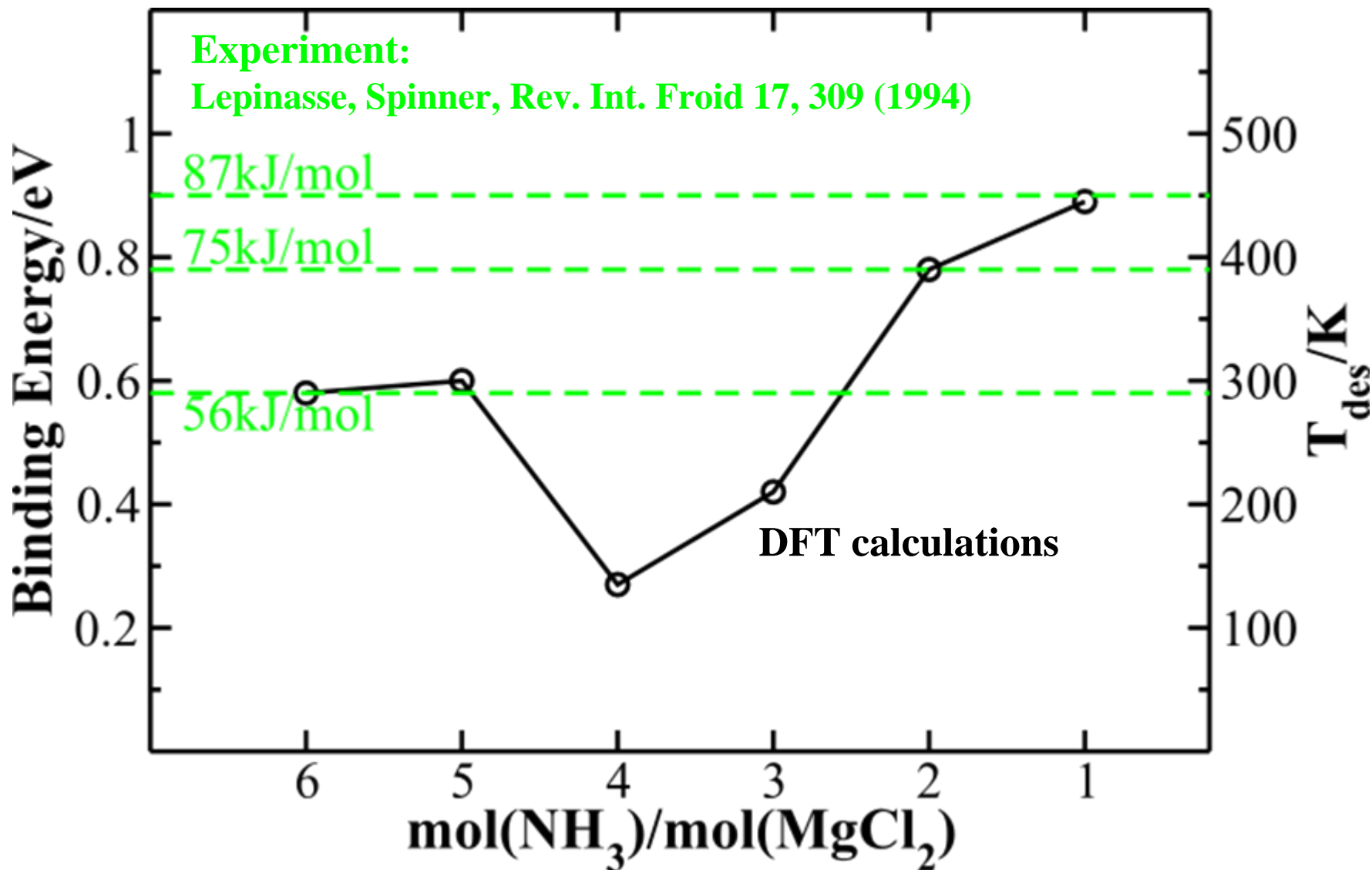
The ammonia content

$Mg(NH_3)_6Cl_2$:	38.1 kmol NH_3 /m ³
Liquid ammonia:	40.1 kmol NH_3 /m ³

Thermal decomposition

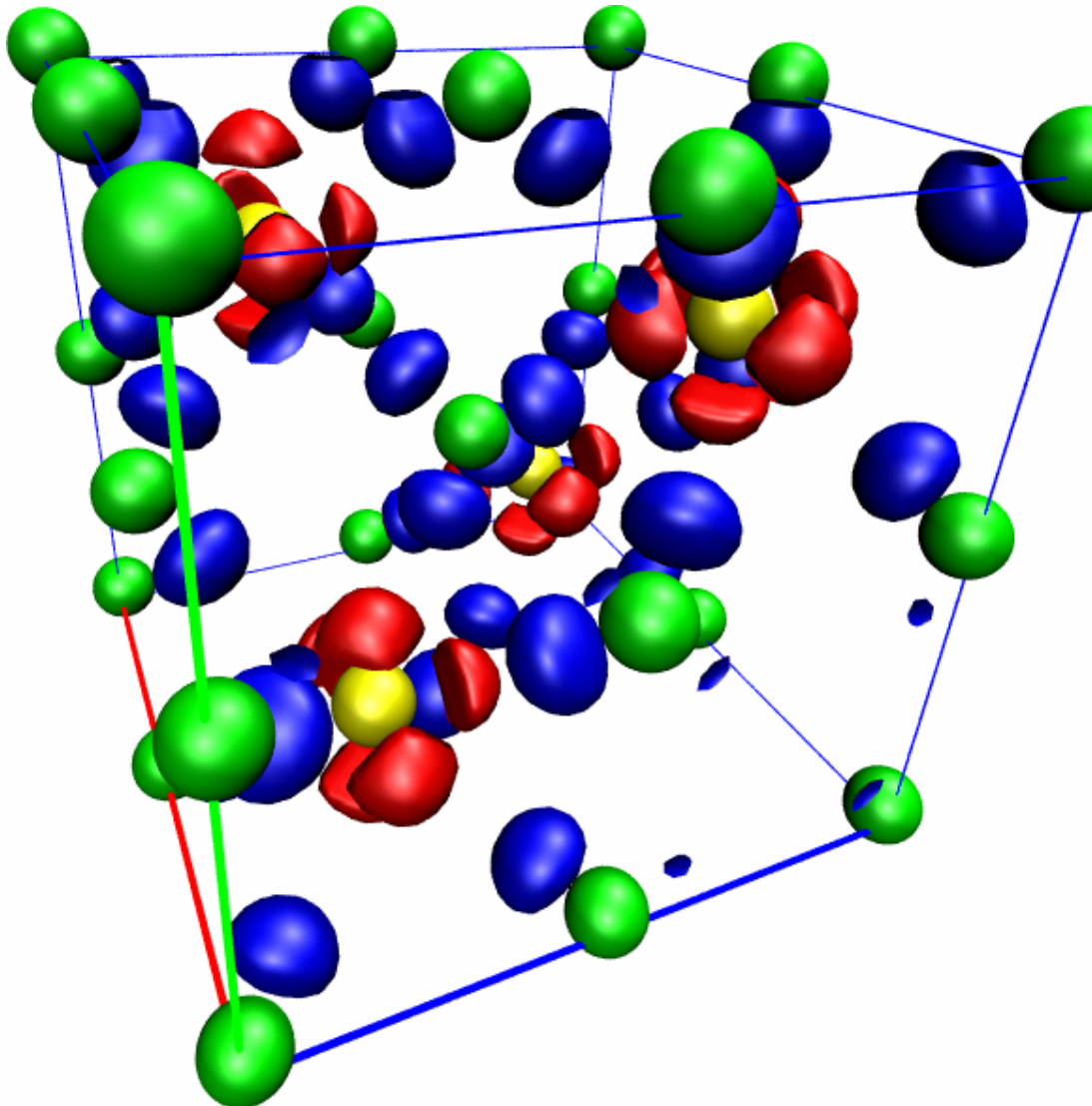


Decomposition of $\text{Mg}(\text{NH}_3)_6\text{Cl}_2$

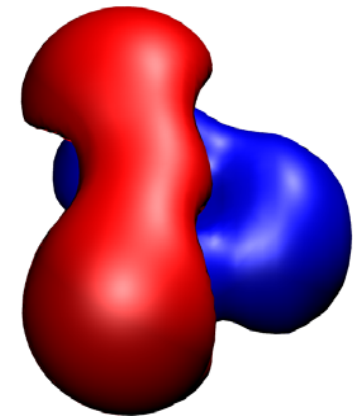


Bonding in metal ammines

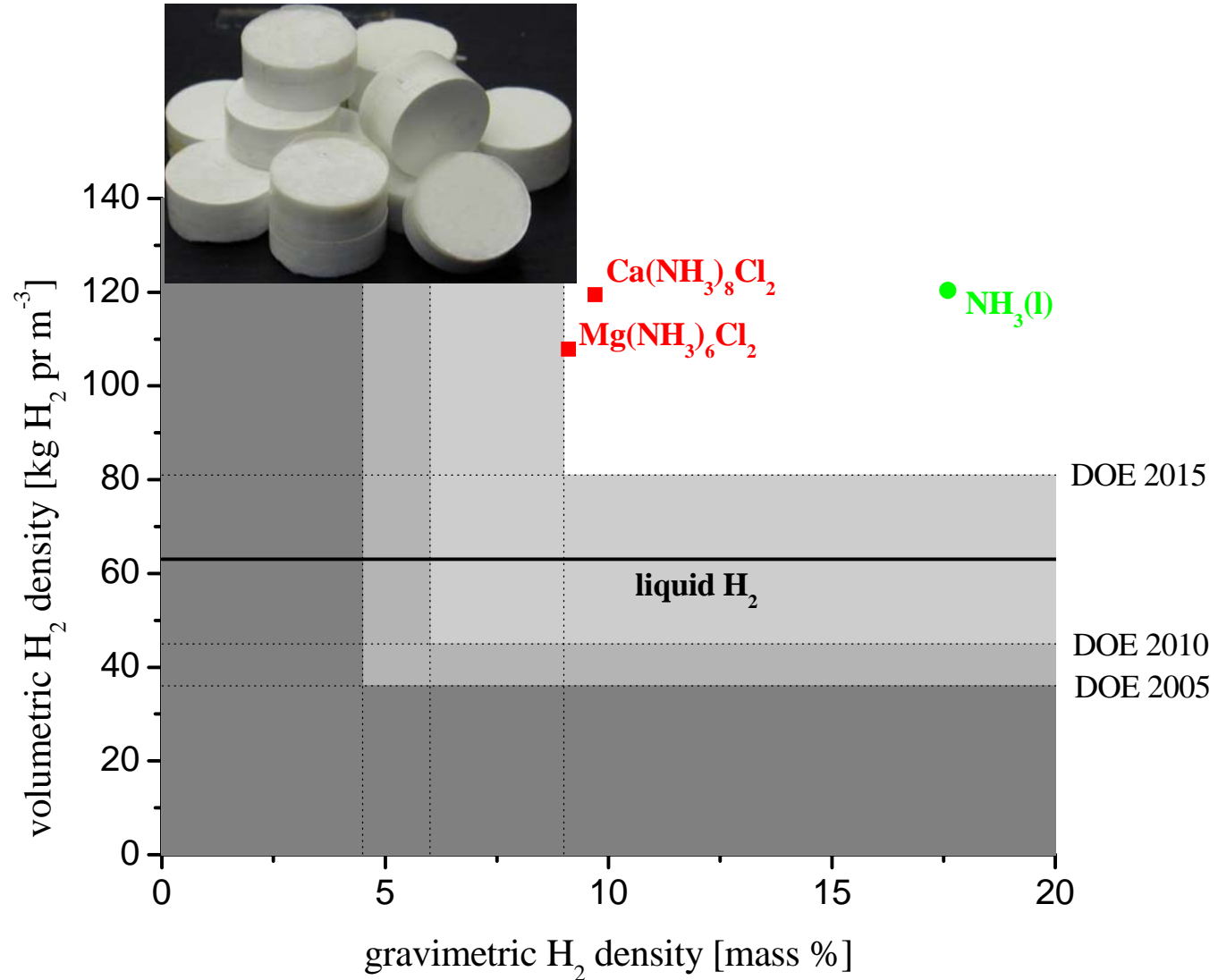
MgCl₂ in Mg(NH₃)₆Cl₂ structure



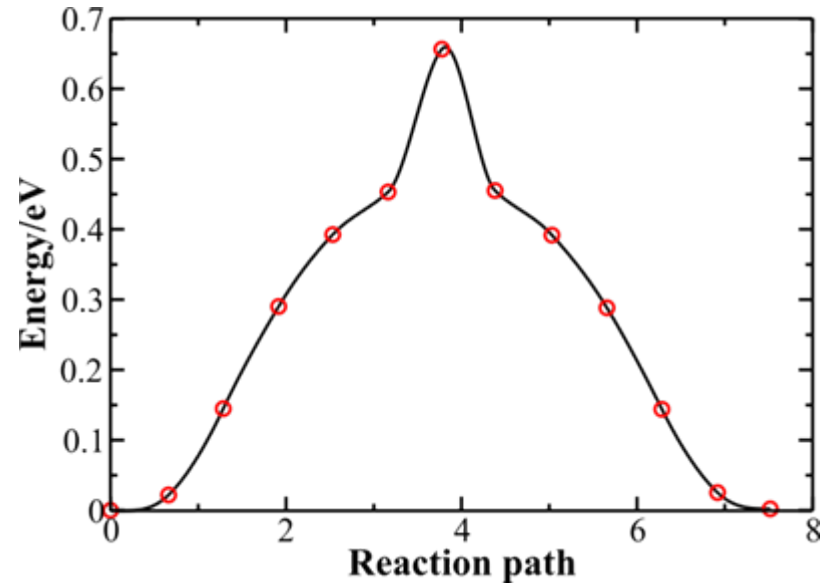
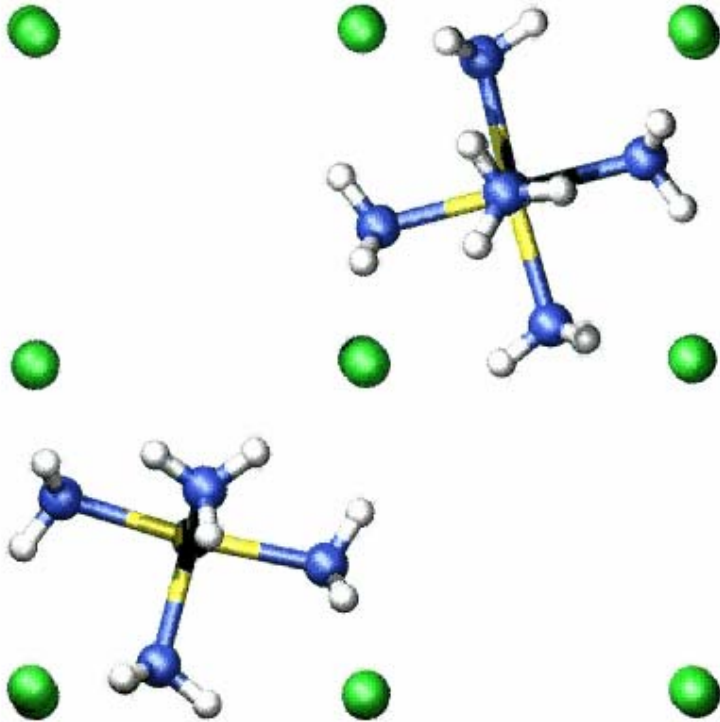
H₃-N



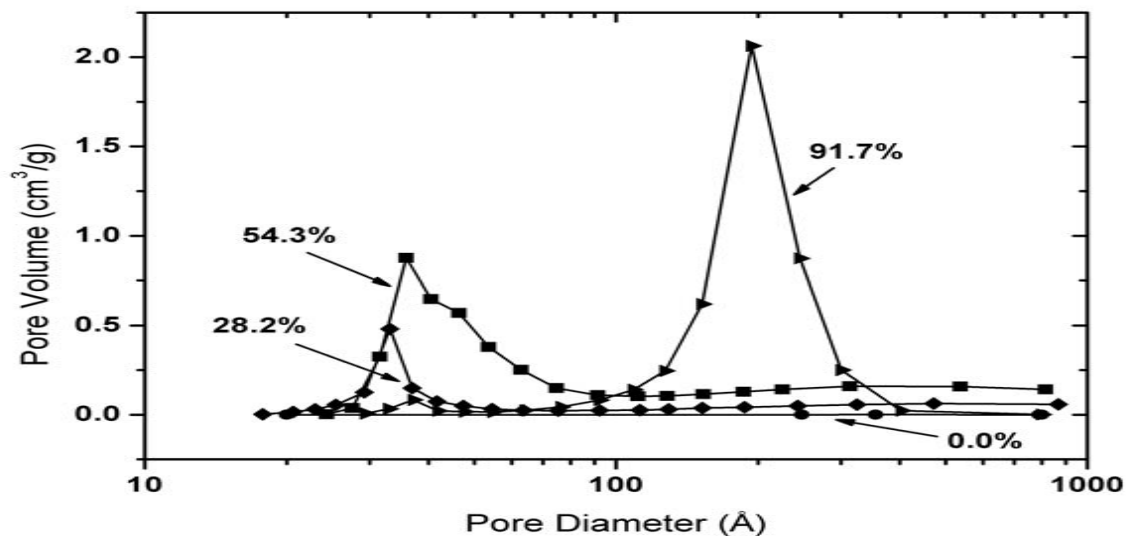
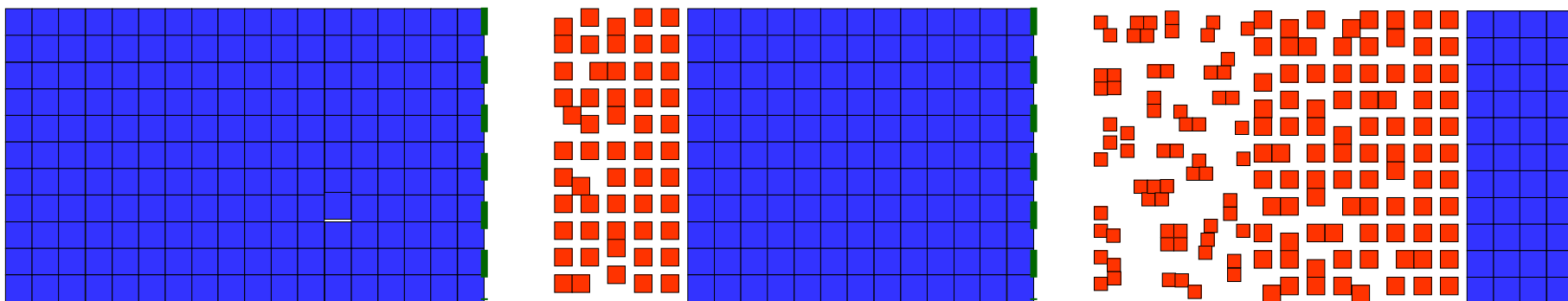
Compacting into a solid



Diffusion in metal ammines



Pore development in dense ammine units



Hummelshøj, Sørensen, Kustova, Johannessen, Nørskov, Christensen, JACS 16, 66 (2006)

> 7% hydrogen below 80 C

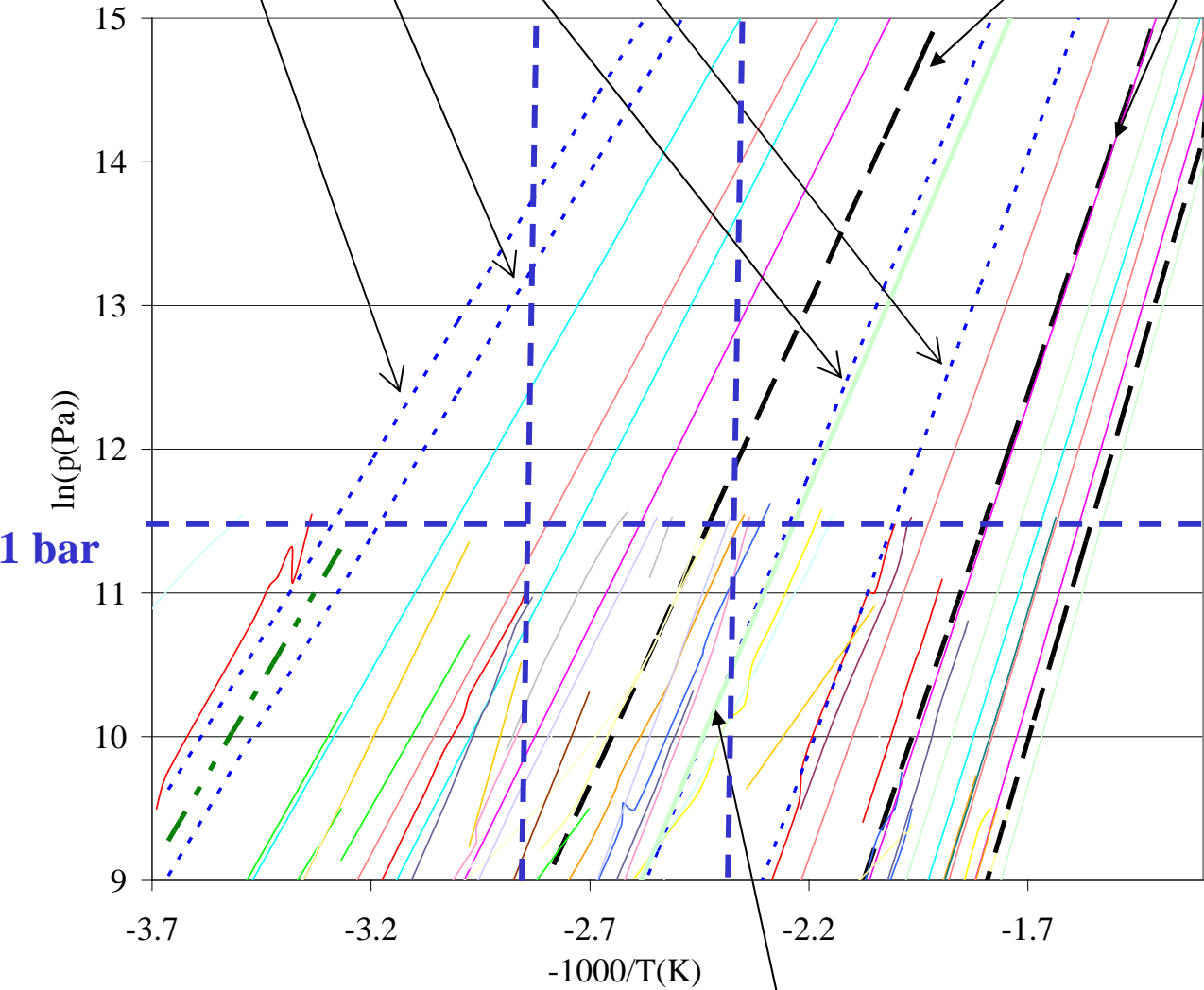
> 6% hydrogen below 150 C

CaCl₂: 8→4; 4→2; 2→1; 1→0

MgCl₂: 6→2; 2→1; 1→0;

80 C

150 C



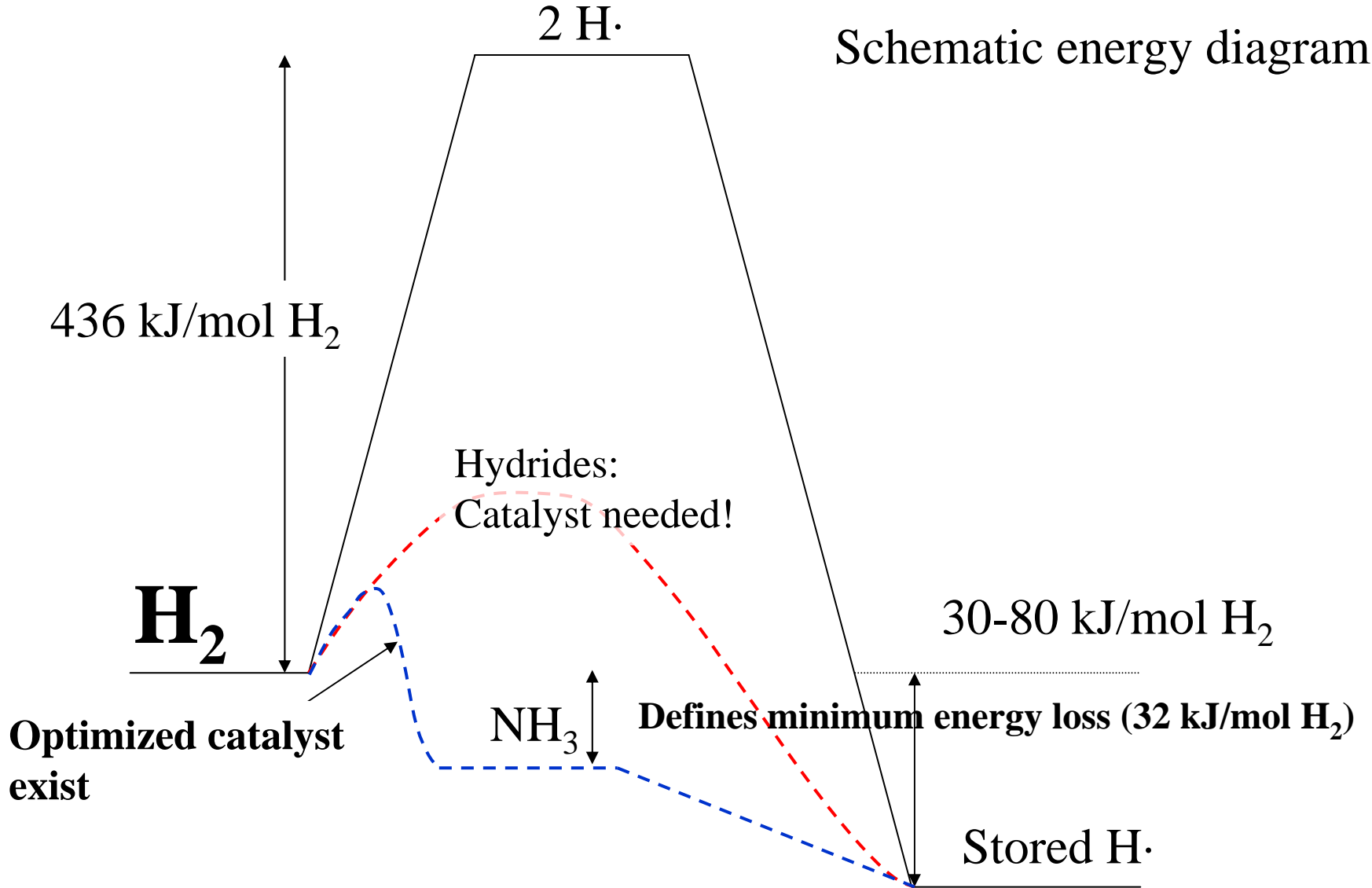
- | | |
|---|---------------------------|
| — MgCl ₂ 6-2 | — MgCl ₂ 2-1 |
| — ZnCl ₂ 6-4 | — ZnCl ₂ 4-2 |
| — ZnCl ₂ 2-1 | — CaBr ₂ 8-6 |
| — CaBr ₂ 6-2 | — CaBr ₂ 2-1 |
| — CaBr ₂ 1-0 | — CaI ₂ 6-2 |
| — CaI ₂ 2-1 | — CaI ₂ 1-0 |
| — BaI ₂ 8-6 | — BaI ₂ 6-4 |
| — BaI ₂ 4-2 | — BaI ₂ 2-0 |
| — FeCl ₂ 6-2 | — FeCl ₂ 2-1 |
| — FeCl ₂ 1-0 | — FeBr ₂ 6-2 |
| — FeBr ₂ 2-1 | — FeBr ₂ 1-0 |
| — FeI ₂ 6-2 | — FeI ₂ 2-0 |
| — CaCl ₂ 8-4 | — CaCl ₂ 4-2 |
| — CaCl ₂ 2-1 | — CaCl ₂ 1-0 |
| — FeSO ₄ 6-4 | — FeSO ₄ 4-3 |
| — SrCl ₂ 8-1 | — SrBr ₂ 8-2 |
| — SrBr ₂ 2-1 | — SrBr ₂ 1-0 |
| — SrI ₂ 8-6 | — SrI ₂ 6-2 |
| — SrI ₂ 2-1 | — SrI ₂ 1-0 |
| — CoCl ₂ 6-2 | — CoCl ₂ 2-1 |
| — CoCl ₂ 1-0 | — MgCl ₂ 1-0 |
| — NH ₄ Cl | — NiCl ₂ 6-2 |
| — NiCl ₂ 2-1 | — NiCl ₂ 1-0 |
| — NiI ₂ 6-2 | — NiSO ₄ 6-2 |
| — Ni(NO ₃) ₂ 6-0 | — MnCl ₂ 6-2 |
| — MnCl ₂ 2-1 | — MnCl ₂ 1-0 |
| — Cu(NO ₃) ₂ 6-4 | — CuCl ₂ 3,3-2 |
| — CuBr ₂ 5-3,3 | — CuBr ₂ 3,3-2 |
| — CuI ₂ 5-3,3 | — CuI ₂ 3,3-2 |
| — CuSO ₄ 5-4 | — CuSO ₄ 4-2 |
| — CuSO ₄ 2-0 | |

NiCl₂: 6→2

Data from: Lepinasse, Spinner, Rev. Int. Froid 17, 309 (1994)

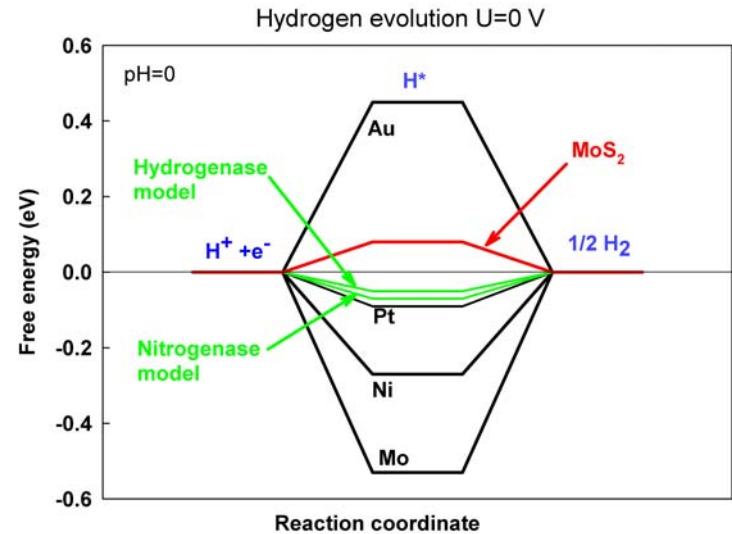
Activating H_2

Schematic energy diagram



Catalysis in hydrogen production and storage

- Catalysis in hydrogen production
 - Understanding of trends in hydrogen and oxygen evolution
 - Towards computational design
 - Inspiration from nature



- Catalysis in hydrogen storage
 - H₂ activation important
 - Alternative combinations of storage medium and catalyst

